



Experimental and modeling study of the mutual oxidation of *N*-pentane and nitrogen dioxide at low and high temperatures in a jet stirred reactor

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ABSTRACT

The mutual oxidation of *n*-pentane and NO₂ at 500–1000 K has been studied at equivalence ratios of 0.5 and 1.33 by using an atmospheric-pressure jet stirred reactor (JSR). *N*-pentane, O₂, NO, NO₂, CO, CO₂, CH₂O, C₂H₄, and CH₃CHO are simultaneously quantified, in-situ by using an electron-impact molecular beam mass spectrometer (EI-MBMS), a micro-gas chromatograph (μ-GC), and a mid-IR dual-modulation faraday rotation spectrometer (DM-FRS). Both fuel lean and rich experiments show that, in 550–650 K, NO₂ addition inhibits low temperature oxidation. With an increase of temperature to the negative temperature coefficient (NTC) region (650–750 K), NO₂ addition weakens the NTC behavior. In 750–1000 K, high temperature oxidation is accelerated with NO₂ addition and shifted to lower temperature. Two kinetic models, a newly developed RMG *n*-pentane/NO_x model and Zhao's *n*-pentane/NO_x model (Zhao et al., 2018, Submitted) were validated against experimental data. Both models were able to capture the temperature-dependent NO₂ sensitization characteristics successfully. The results show that although NO₂ addition in *n*-pentane has similar effects to NO at many conditions due to fast NO and NO₂ interconversion at higher temperature, it affects low temperature oxidation somewhat differently. When NO₂/NO interconversion is slow, NO₂ is relatively inert while NO can strongly promote or inhibit oxidation.

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1. Introduction

Due to the increasing use of the exhaust gas recirculation (EGR) technique to reduce combustion pollutants in different types of internal engines, the effect of exhaust burned-gases (CO₂, H₂O, NO_x, etc.) on the ignition characteristics has received a lot of attention [1–5]. It is well known that trace amounts of NO_x from EGR can significantly alter the ignition kinetics at both low and high temperatures [6,7]. The sensitization effect of NO on fuel (alkane, alcohol, aromatics, ether, etc.) oxidation has been studied in jet stirred reactors (JSR), flow reactors (FR), and homogeneous charge compression ignition (HCCI) engines [6–13]. NO addition inhibits and promotes fuel oxidations at lower and higher temperatures, respectively. The temperature-dependent radical propagation and

termination reactions, NO + HO₂ = NO₂ + OH, NO + RO₂ = RO + NO₂, and NO + OH + M = HONO + M mainly explain the temperature-dependent NO sensitization characteristics, where R represents the fuel radical [6,7,10]. Our recent work [13] studied the NO sensitization effect on low temperature oxidation of *n*-pentane. It was observed that NO addition delayed the onset temperature of low temperature oxidation, suppressed the negative temperature coefficient (NTC) behavior, and shifted the high temperature oxidation to lower temperature.

However, as much as 20%–40% of the NO_x emission from diesel and gasoline engines at moderate loads is in the form of NO₂ [14,15]; therefore, the kinetic effect of NO₂ from EGR on engine ignitions is also of importance. The NO₂ sensitization effect on oxidation of hydrogen, methane, methanol, and benzene has been investigated in FR [16–19], JSR [20,21] and shock tube [22] at high temperatures. It was shown that NO₂ addition enhanced high temperature fuel oxidations and lowered the high temperature ignition temperature by altering the H₂/O₂ chemistry. However, to

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List of abbreviations

DM-FRS	Dual-modulation faraday rotation spectrometer
EGR	Exhaust gas recirculation
EI-MBMS	Electron-impact molecular beam mass spectrometer
FR	Flow reactor
HCCI	Homogeneous charge compression ignition
JSR	Jet stirred reactor
MKS	Mass flow controller
NTC	Negative temperature coefficient
QSS	Quasi-steady-state
RMG	Reaction Mechanism Generator
μ -GC	Micro-gas chromatograph

the author's knowledge, there are few kinetic studies available on the mutual oxidation of NO₂ and larger alkanes, like gasoline or diesel representatives. Especially, the effect of NO₂ addition on low temperature oxidation is not emphasized. In addition, as one of the simple alkanes with low temperature reactivity, *n*-pentane has been proved to be a good test fuel to study the NO_x sensitization effect on its oxidation [13,23–25].

Motivated by the above discussion, the present paper aims to study the NO₂ sensitization effect on *n*-pentane oxidation at both low and high temperatures, especially to understand its impact on the onset temperature of low temperature oxidation, the transition of NTC behavior, and the high temperature ignition. The experiments of *n*-pentane oxidation with and without 250 ppm NO₂ addition were performed at both lean and rich conditions at 500–1000 K in an atmospheric-pressure JSR. The mole fractions of *n*-pentane, O₂, CO, CO₂, NO, NO₂, CH₂O, C₂H₄, and CH₃CHO were simultaneously quantified in-situ by using a mid-IR dual-modulation faraday rotation spectrometer (DM-FRS), an electron-impact molecular beam mass spectrometer (EI-MBMS), and a micro-gas chromatograph (μ -GC). Zhao's *n*-pentane/NO_x model [13] and a new *n*-pentane/NO_x model, developed by the open-source automated Reaction Mechanism Generation (RMG) software [26,27], were used to predict the temperature evolution of major and intermediate species and analyze the temperature-dependent NO₂ sensitization characteristics.

2. Experimental methods and kinetic models

A spherical fused silica JSR with an internal volume of 42 cm³ was used in this study. It has four finger injectors with a 1 mm inner diameter to generate intense turbulence for homogenous mixing [13,28,29]. The JSR is covered by a stainless-steel jacket with a three-stage-regulated heating system to maintain a good thermal homogeneity throughout the reactor. The operating temperature is up to 1300 K. Volumetric flow rates of gases (O₂, Ar, N₂, and NO₂) and liquid (*n*-pentane) were, respectively, regulated by four mass flow controllers (MKS) and a syringe pump (Harvard Apparatus, PHD 22/2000). A secondary nitrogen stream, which carried vaporized *n*-pentane in the pre-vaporizer to the JSR entrance, was mixed with the primary gas stream (O₂/Ar/N₂/NO₂). The temperature uniformity is within ± 3 K along the vertical axis of the reactor from 500 to 1000 K. Gas samples were taken by sonic probes at the exit of the JSR and analyzed by EI-MBMS, μ -GC, and DM-FRS simultaneously with cross-validation.

An EI-MBMS was employed to measure major species with a mass resolution of around 900. Gas and liquid species were calibrated directly by flowing the mixture with known mole fractions

in excess N₂ and Ar. Details of the EI-MBMS and species calibrations are described elsewhere [5,30,31]. Species calibrations and the electron impact (20 \pm 1 eV) in the MBMS mainly account for the measurement uncertainty of \sim 10–20%. A μ -GC (Inficon 3000) was also used to quantify stable combustion species within a 5% uncertainty. The description of the μ -GC module is given elsewhere [32,33]. A DM-FRS system, developed at Princeton, was used to measure the NO content at the outlet of the JSR within a 5% uncertainty [34,35]. It targeted the ¹⁴N¹⁶O P(19/2)_e doublet transition at 1842.946 cm⁻¹ (major isotope) of NO. A laser-intensity-independent and etalon-free measurement was obtained by modulating both the applied magnetic field and the laser current. The detection limit of NO in the DM-FRS system is \sim 1 ppb. Further details are available elsewhere [13,34–36].

The experiments were performed at both fuel lean and rich conditions ($\phi = 0.5$ and 1.33) with and without 250 ppm NO₂ additions at 500–1000 K and atmospheric pressure. Experimental conditions are shown in Table 1. The fuel concentration was fixed at 1% with varied O₂ mole fractions. The inlet volume flow rate is fixed at 969 ml/min at 295 K, as such, the residence time in the reactor varies with temperature (Table 1).

A newly developed RMG *n*-pentane/NO_x model and Zhao's *n*-pentane/NO_x model [13] were used to predict the experimental data in this paper. Zhao's model consists of an *n*-pentane mechanism from the AramcoMech [24] and an updated NO_x sub-mechanism developed at Princeton [13]. Details of Zhao's model as well as the NO_x sub-mechanism is described elsewhere [13].

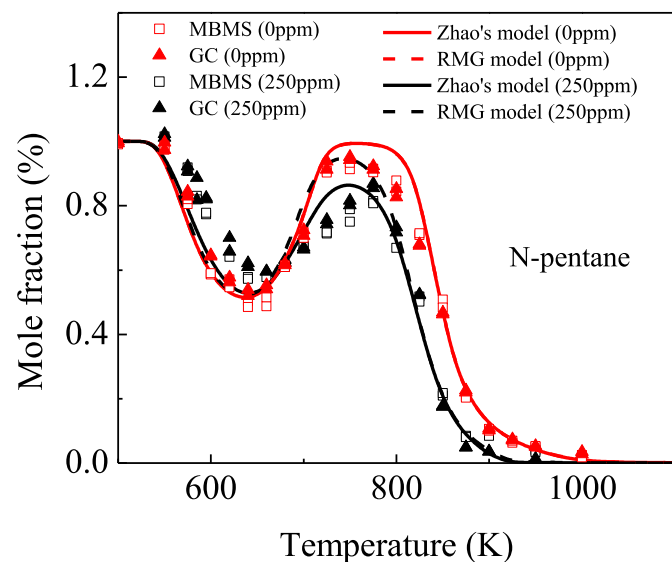
The RMG model was obtained by relying on the *n*-pentane AramcoMech kinetic framework [24], and additional reaction subsets generated using the open-source automated Reaction Mechanism Generation software v2.1.0 [26,27]. While generating this model, particular attention was given to reactions of NO/NO₂ affecting the concentrations of oxy (RO) and peroxy (RO₂) radicals in the system. Specifically, more than eighty RO + NO = RONO = R + NO₂ (including RO₂ + NO = ROONO = RO + NO₂) reactions were automatically generated and included in the model for various RO and RO₂ radicals in the system. The reaction rates were derived from the "Radical Recombination" reaction family of RMG, and relevant thermodynamic properties of intermediates were estimated by RMG using Benson's group additivity method [37]. Another subset includes NO₂ + RH = HONO + R reactions, of which more than 100 entries were generated by the "Hydrogen Abstraction" reaction family of RMG. An additional NO_x sub-mechanism was built based on the kinetic data reported in the seminal review by Dean and Bozzelli [38] with relevant updates and additions from the RMG NO_x library. In other words, both the RMG model and Zhao's model share the same *n*-pentane base mechanism, but have different NO_x chemistry subsets. Moreover, Zhao's model has only three RO + NO pathways. The RMG model gives an improved prediction of the onset temperature of the low temperature mutual oxidation of *n*-pentane and NO in the experiment of [13] (see Fig. S1 in the supplementary document). Several reactions were modified in Zhao's model [13] from their original values (Table S1 in the supplementary document), and these modified values were kept in the RMG model. Simulations were performed in the perfectly stirred reactor module of CHEMKIN software [39].

3. Results and discussion

The temperature evolution of *n*-pentane mole fraction at the fuel lean conditions ($\phi = 0.5$) with and without 250 ppm NO₂ addition is shown in Fig. 1. The low temperature oxidation of *n*-pentane is clearly observed in the experiment. EI-MBMS and μ -GC measurements agree within 10%. Both Zhao's model and the RMG model predict the temperature evolution of *n*-pentane oxidation

Table 1
Experimental conditions.

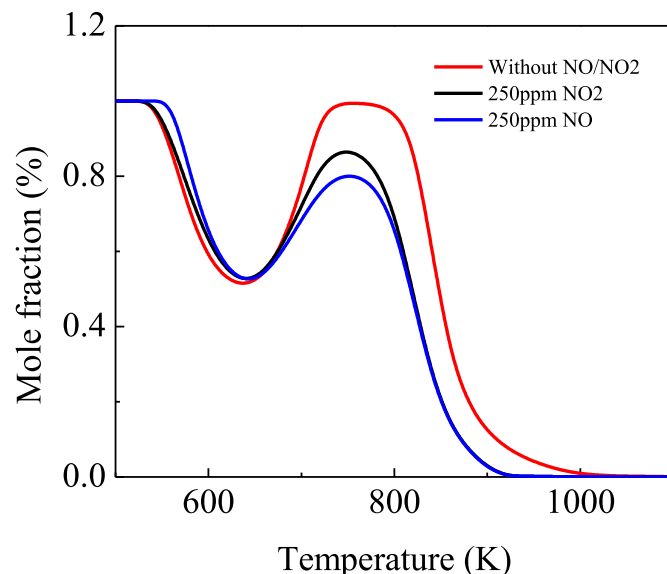
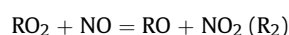
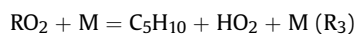
Case	Equivalence ratio	N-C ₅ H ₁₂ (%)	O ₂ (%)	Ar (%)	N ₂ (%)	NO ₂ (ppm)	Residence time (s)	Temperature (K)
1	0.5	1	16	5	78	0	1.53–0.77	500–1000
2	0.5	1	16	5	77.975	250	1.53–0.77	500–1000
3	1.33	1	6	5	88	0	1.53–0.77	500–1000
4	1.33	1	6	5	87.975	250	1.53–0.77	500–1000

**Fig. 1.** Temperature evolution of the mole fraction of *n*-pentane at the fuel lean conditions ($\phi = 0.5$) with and without 250 ppm NO₂ addition in a JSR, conditions of Table 1.

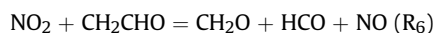
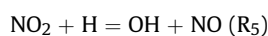
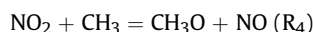
without NO₂ addition reasonably well as expected since they are both based on the *n*-pentane model of [24] which was adjusted to match JSR data on *n*-pentane. With 250 ppm NO₂ addition, it is seen that NO₂ sensitizes the oxidation significantly. Firstly, NO₂ slows down low temperature oxidation in 550–650 K, but does not change the onset temperature of low temperature oxidation. Secondly, NO₂ suppresses the NTC behavior in the NTC region (650–750 K). Furthermore, NO₂ shifts high temperature oxidation to lower temperature in the intermediate and high temperature region (750–1000 K).

The NO sensitization effect on *n*-pentane oxidation has been investigated in our previous study [13]. In this paper, the *n*-pentane oxidation at fuel lean conditions with the same doping concentration of NO and NO₂ are compared to simulations in Fig. 2. It is seen that both NO and NO₂ additions show the three similar sensitization characteristics in low and intermediate temperatures. However, when the normal oxidation chain branching is suppressed, NO₂ addition has less effect on fuel oxidation. In addition, NO addition delays the onset temperature of *n*-pentane low temperature oxidation, while NO₂ has little effect on the onset temperature.

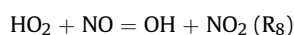
To explain the impact of NO₂ addition on *n*-pentane oxidation at low and high temperatures, pathway analyses of *n*-pentane and NO₂ were respectively performed at 600, 700, and 800 K by using the RMG model at the lean condition with 250 ppm NO₂ addition (Figs. 3–5). The pathway analysis of *n*-pentane in Fig. 3 shows that there are three reaction channels of RO₂ consumption,

**Fig. 2.** Temperature evolution of the mole fraction of *n*-pentane at the fuel lean conditions ($\phi = 0.5$) with 250 ppm NO₂, with 250 ppm NO, and without NO₂/NO additions using Zhao's model.

Reaction R₁ is part of the typical low temperature oxidation channel, which proceeds through competing reactions between QOOH decomposition and QOOH + O₂. Reaction R₂ describes RO₂ consumption by NO, and reaction R₃ is a decomposition channel forming HO₂. Since RO and HO₂ (produced in reaction channels R₂ and R₃) are much less reactive than OH radicals (produced from QOOH subsequent reaction R₁) at low temperature, reaction channels R₂ and R₃ (Fig. 3, red and green pathways) play inhibiting roles in *n*-pentane oxidation in 550–650 K. As for NO₂-related pathways, it is noted that NO and HONO are produced from NO₂, respectively, mainly through reactions R₄–R₇,



while at low temperature, NO reacts with RO₂ and HO₂ to regenerate NO₂ quickly through reactions R₂ and R₈, respectively.



Therefore, according to the pathway analysis, NO and HONO are a quasi-steady-state (QSS) species and a stable species at low temperature, respectively, and the rates of interconversion among

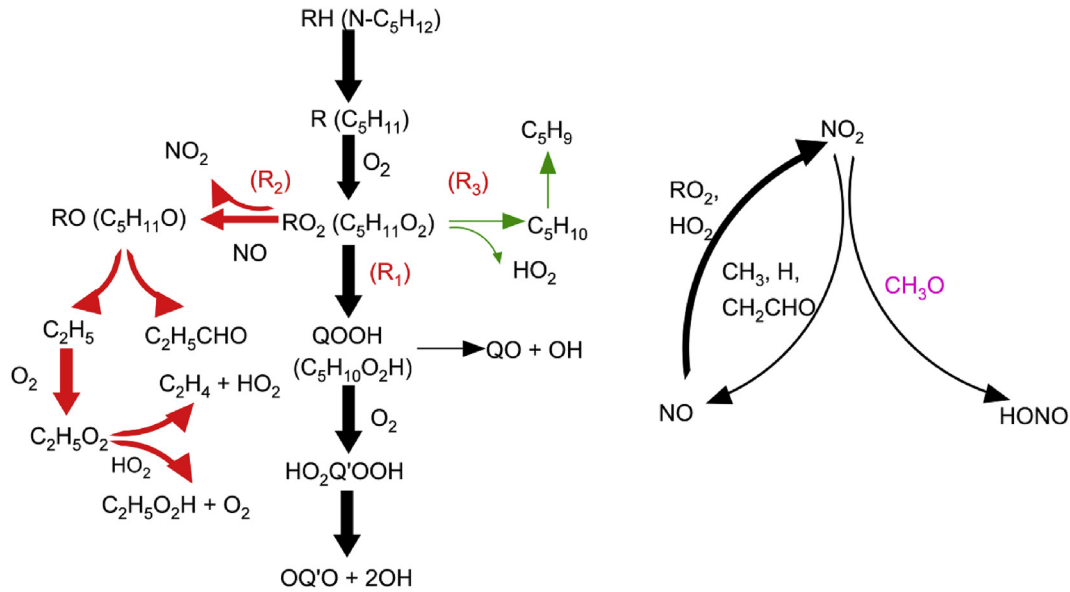


Fig. 3. Pathway analysis of *n*-pentane and NO_2 at 600 K for a JSR in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model.

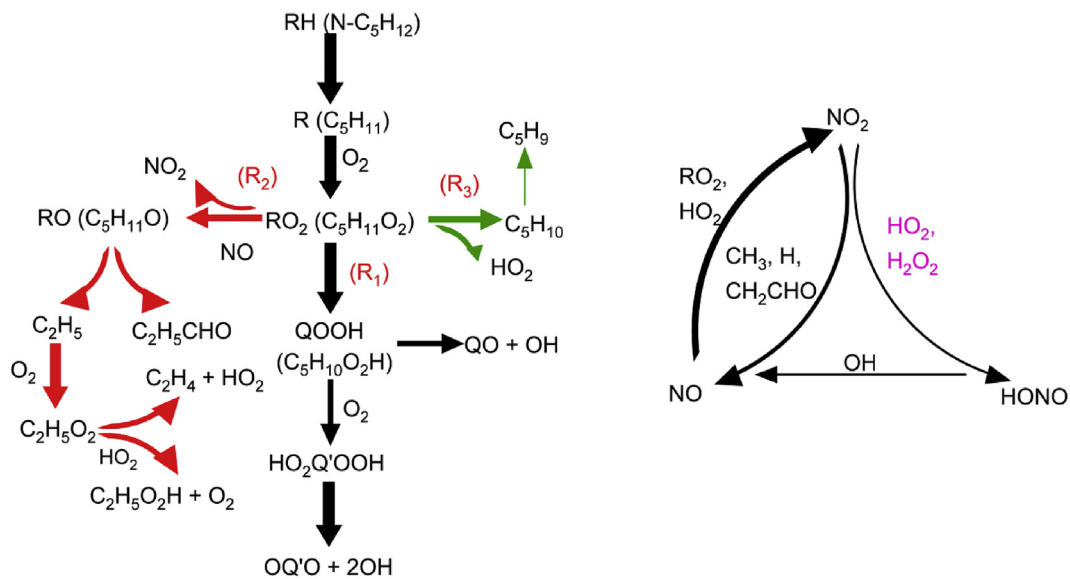
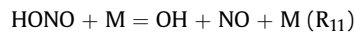


Fig. 4. Pathway analysis of *n*-pentane and NO_2 at 700 K for a JSR in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model.

NO , NO_2 , and HONO are quantified below in terms of reaction characteristic time scales (Fig. 11). Reaction channel R_1 (Fig. 3, black pathway) promotes low temperature oxidation of *n*-pentane through the formation of QOOH , O_2QOOH , and subsequent two OH radicals. However, with 250 ppm NO_2 addition, NO is produced from NO_2 mainly through reactions R_4 – R_6 , and then immediately consumes RO_2 and HO_2 through the inhibiting reaction channel R_2 and R_3 (Fig. 3, red and green pathways), competing with R_1 (Fig. 3, black pathway). Therefore, the reactivity slows down.

In the NTC region in Fig. 4, the pathway analysis of NO_2 shows that HONO , produced from reaction R_9 and R_{10} , begins to decompose to NO through R_{11} ,



and NO is still a QSS species, which is also clarified in terms of reaction characteristic time scales in Fig. 11. The combination of R_9 and R_{11} converts a relatively inactive radical, HO_2 , into a very active OH radical, and the additional NO generated by R_{11} does the same thing via R_8 . This also reduces radical loss via $\text{HO}_2 + \text{HO}_2$, which is very important in NTC [40]. Hence, reactivity increases, and NO_2 addition partially suppresses NTC behavior.

With an increase of temperature to 800 K in Fig. 5, reaction channel R_3 (Fig. 5, green pathway) plays a dominant role of the RO_2 consumption in the pathway analysis of *n*-pentane. A significant dissociation of HONO into OH and NO through reaction R_{11} in the pathway analysis of NO_2 also occurs. Without NO_2 , reaction channel R_3 (Fig. 5, green pathway) suppresses the oxidation as HO_2 is relatively stable. However, when NO_2 is added, two OH radicals are

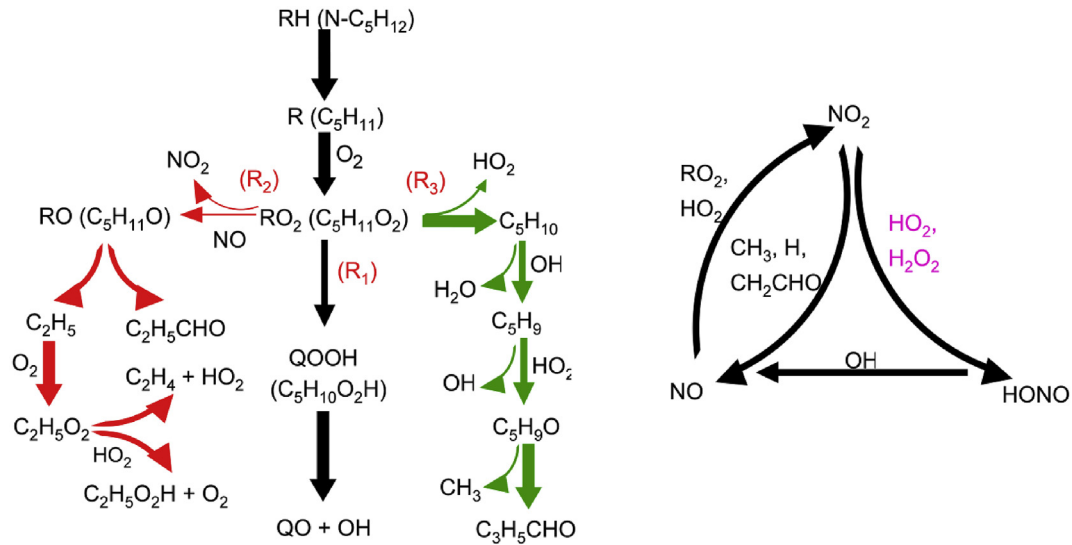


Fig. 5. Pathway analysis of *n*-pentane and NO_2 at 800 K in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model.

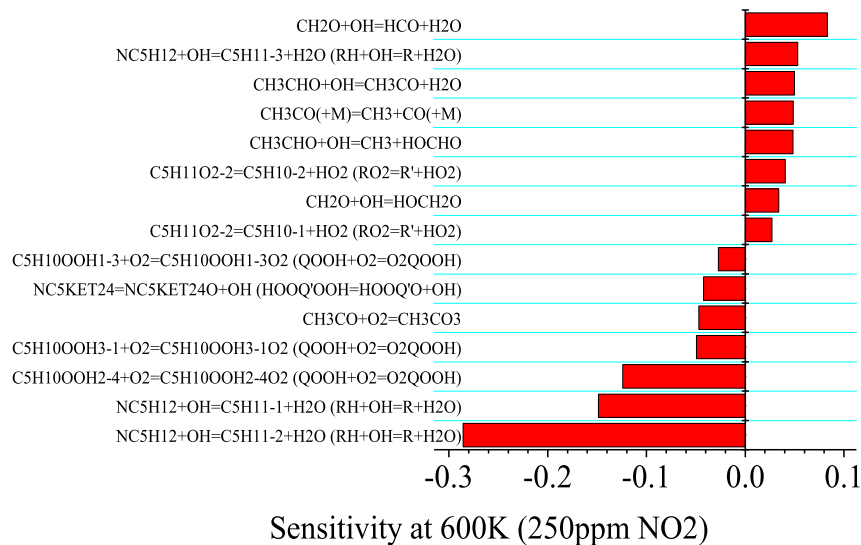
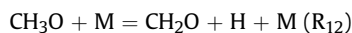


Fig. 6. Sensitivity analysis of *n*-pentane in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model in a JSR at 600 K, conditions of Table 1.

overall formed from two HO_2 radicals through the reaction series R_8 – R_{11} in reaction channel R_3 , promoting the oxidation. In addition, CH_3 , produced in the pathway of reaction channel R_3 (Fig. 5, green pathway), forms H and OH radicals through this series of reactions.



This also contributes to the promoting effect of NO_2 in the intermediate and high temperature region.

Based on the discussion above, the NO_x effect on alkene oxidation may be interpreted as following.

- When the oxidation is running at the temperatures with enough HO_2 and OH radicals, NO_x behaves as a catalyst, and the catalytic cycle time $\text{NO}_2 \rightarrow \text{NO} \rightarrow \text{NO}_2$ is relatively short compared to the residence time in the reactor.
- At conditions where the normal oxidation chain branching is suppressed, the NO_x interconversion is slow enough that the system is sensitive to which species, NO or NO_2 , is introduced. NO_2 addition has less effect on the oxidation at these conditions than NO because R_2 and R_8 are always fast but some of the NO_2 reactions are slow.

To cross-validate the pathway analyses, the sensitivity analyses of the *n*-pentane mole fraction at the fuel lean condition with 250 ppm NO_2 addition were also performed at 600, 700, and 800 K, respectively, by using the RMG model (Figs. 6–8). It can be seen from Fig. 6 that the H abstraction reactions of *n*-pentane, HOOQ'OOH decomposition reaction, QOOH addition reaction with O_2 , and the RO_2 decomposition reactions are the most sensitive reactions at 600 K. It is known that the H abstraction reactions of fuels

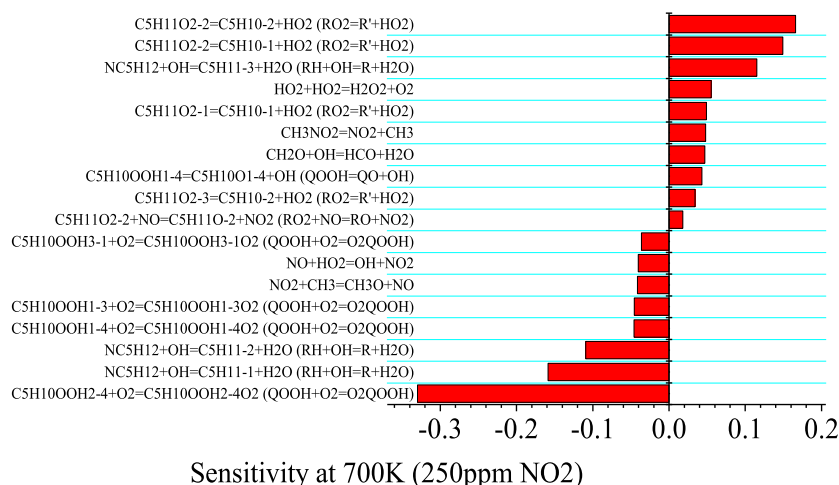


Fig. 7. Sensitivity analysis of *n*-pentane at 700 K in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model in a JSR, conditions of Table 1.

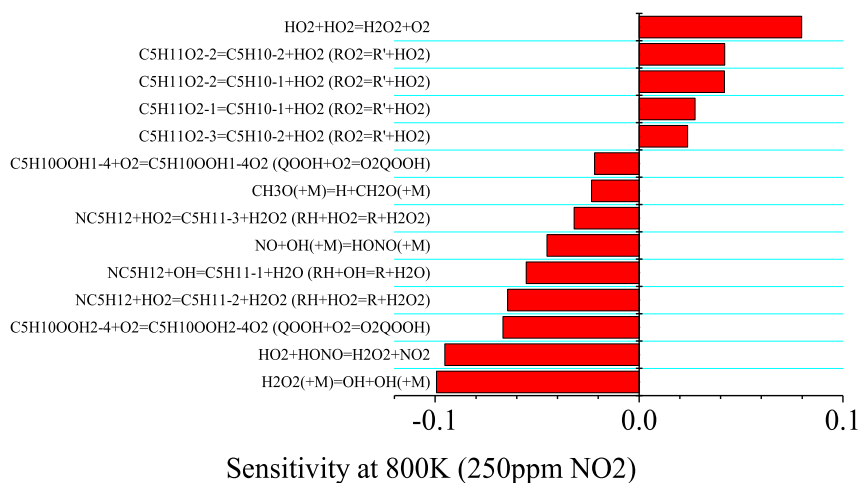


Fig. 8. Sensitivity analysis of *n*-pentane at 800 K in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO_2 addition using the RMG model in a JSR, conditions of Table 1.

generally rank high in the sensitivity analysis. The latter two sets of reactions belong to the reaction channels R_1 and R_3 of RO_2 consumption. At 700 K, the sensitivity analysis in Fig. 7 shows that the most sensitive reactions are the H abstraction reactions of *n*-pentane, reactions through the three RO_2 consumption channels R_1 – R_3 , and NO_2/NO conversion reactions (R_8 and R_{12}). Therefore, in the NTC region, all of the three reaction channels of RO_2 consumption are of importance and affect *n*-pentane oxidation. With an increase of temperature to 800 K, the H abstraction reactions of *n*-pentane by HO_2 and OH, the decomposition of RO_2 to make HO_2 through R_3 , NO_2/NO conversion reactions (R_8 , R_9 , and R_{11}), and reactions of $\text{HO}_2/\text{H}_2\text{O}_2$ chemistry are the most sensitive reactions. At this temperature, chain branching mainly occurs via reactions involving $\text{HO}_2/\text{H}_2\text{O}_2$ through R_9 and R_{10} rather than the QOOH cycle which is dominant at lower T. It is noted that only reaction channel R_3 is the main RO_2 consumption pathway in the sensitivity analysis at 800 K, which is in agreement with the pathway analysis at 800 K (Fig. 5).

Fig. 9 (a)–(d) shows the temperature evolutions of NO_2 , NO, CO, and CO_2 at fuel lean condition ($\phi = 0.5$), respectively. Generally, both Zhao's model and the RMG model have captured the major species temperature evolutions well. However, the models predictions of the NO and NO_2 evolution curves at intermediate and

high temperatures are shifted to higher temperatures. This might be related to uncertainties in pathways of RO_2+NO and NO_2/NO interconversion reactions. It is noted that the temperature evolutions of NO_2 and NO in Fig. 9 (a) and (b) correspond to the pathway analyses of NO_2 at 600, 700, and 800 K. According to the RMG model, the major nitrogen-related species in the oxidation are NO, NO_2 , and HONO. The pathway analysis of NO_2 at 600 K (Fig. 3) shows that HONO is accumulated through reaction R_7 , while NO is a quasi-steady-state species. This explains why the NO_2 concentration dramatically decreases with temperature and NO is experimentally unobservable at 550–650 K in Fig. 9 (a) and (b), respectively. With an increase of temperature to the NTC region, HONO begins to decompose to NO through reaction R_{11} . Thus, NO_2 concentration recovers at 650–750 K in the experiment. Above 750 K, as CH_3 and HO_2 concentrations dramatically increase with temperature, NO_2 consumption through reactions R_4 , R_9 , and R_{10} increases accordingly. Meanwhile, HONO decomposition rate (reaction R_{11}) also increases significantly with temperature. Therefore, the NO_2 concentration decreases while NO begins to accumulate with temperature.

To clarify the model prediction uncertainty of NO_2 at intermediate temperatures (700–800 K), the sensitivity analysis of the NO_2 mole fraction at the fuel lean condition with 250 ppm NO_2 addition

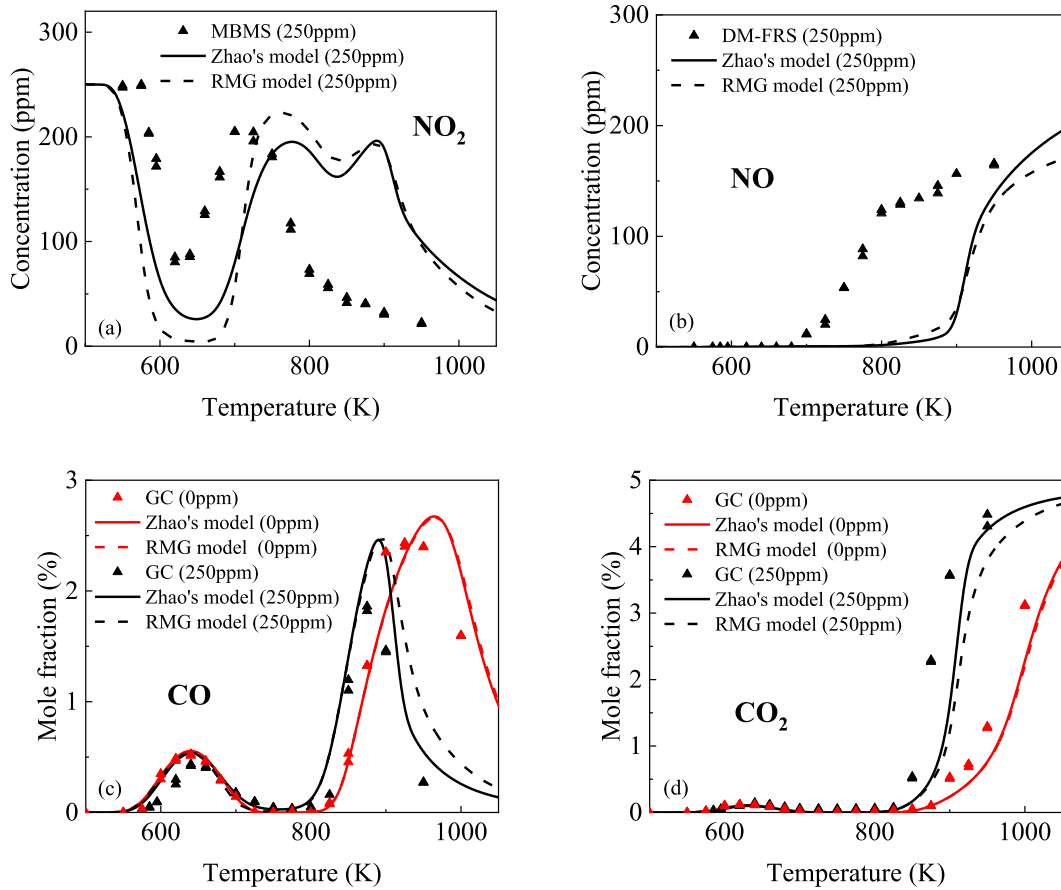


Fig. 9. Temperature evolutions of the concentrations of NO₂, NO, CO, and CO₂ at the fuel lean conditions ($\phi = 0.5$) with and without 250 ppm NO₂ addition in a JSR, conditions of Table 1.

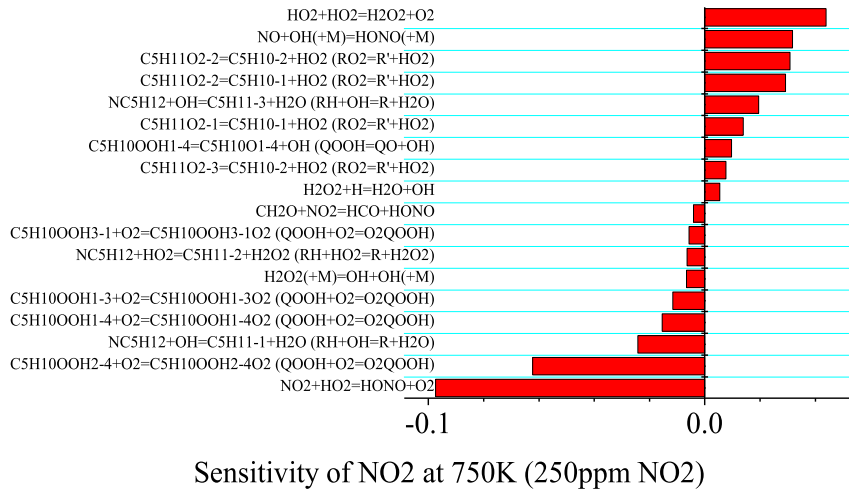


Fig. 10. Sensitivity analysis of NO₂ at 750 K in the fuel lean condition ($\phi = 0.5$) with 250 ppm NO₂ addition using the RMG model in a JSR, conditions of Table 1.

was also performed at 750 K by using the RMG model (Fig. 10). It is seen that the H abstraction reactions of *n*-pentane, QOOH addition reaction with O₂, the RO₂ decomposition reactions, reactions of HO₂/H₂O₂ chemistry, and NO₂/HONO/NO conversion reactions (R₉, R₁₁, and R₁₃) are the most sensitive reactions at this temperature range. Therefore, the main uncertainty may come from the NO_x sub-model, especially involving in HONO chemistry. Quantification

of HONO is necessary to verify the model uncertainty in predicting nitrogen-containing species in the future study.

Furthermore, characteristic time scales of NO, NO₂, and HONO interconversion reactions are compared at different temperatures at the fuel lean condition with 250 ppm NO₂ addition using The RMG model in Fig. 11. According to the discussion above, NO mainly forms NO₂ through reactions R₂ and R₈; NO₂ forms NO through R₄-

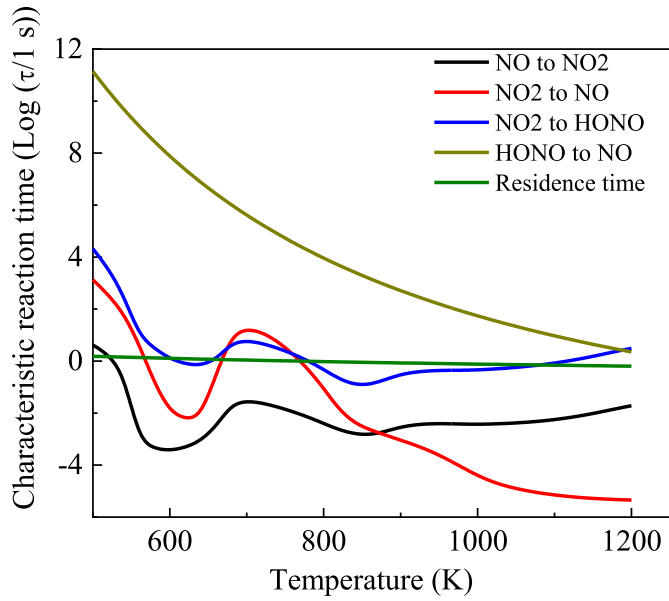


Fig. 11. Temperature evolutions of characteristic time scales of NO, NO₂, and HONO interconversion reactions at the fuel lean conditions ($\phi=0.5$) with 250 ppm NO₂ addition using the RMG model in a JSR, conditions of Table 1.

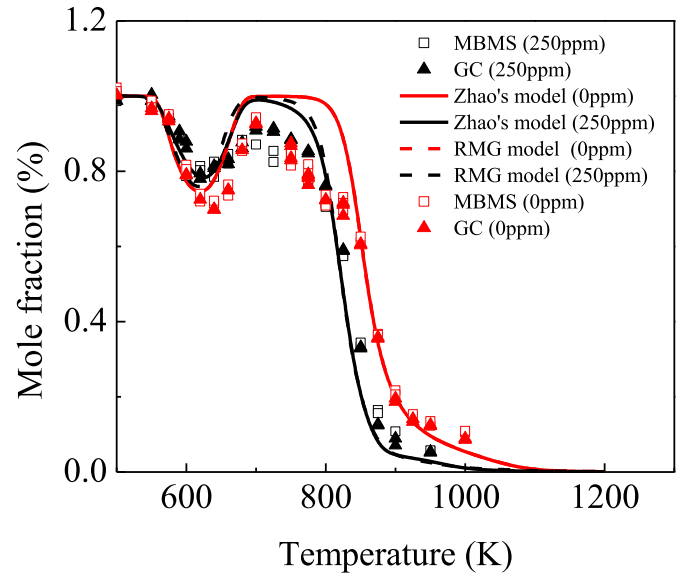


Fig. 13. Temperature evolution of the mole fraction of *N*-pentane at the fuel rich conditions ($\phi=1.33$) with and without 250 ppm NO₂ addition in a JSR, conditions of Table 1.

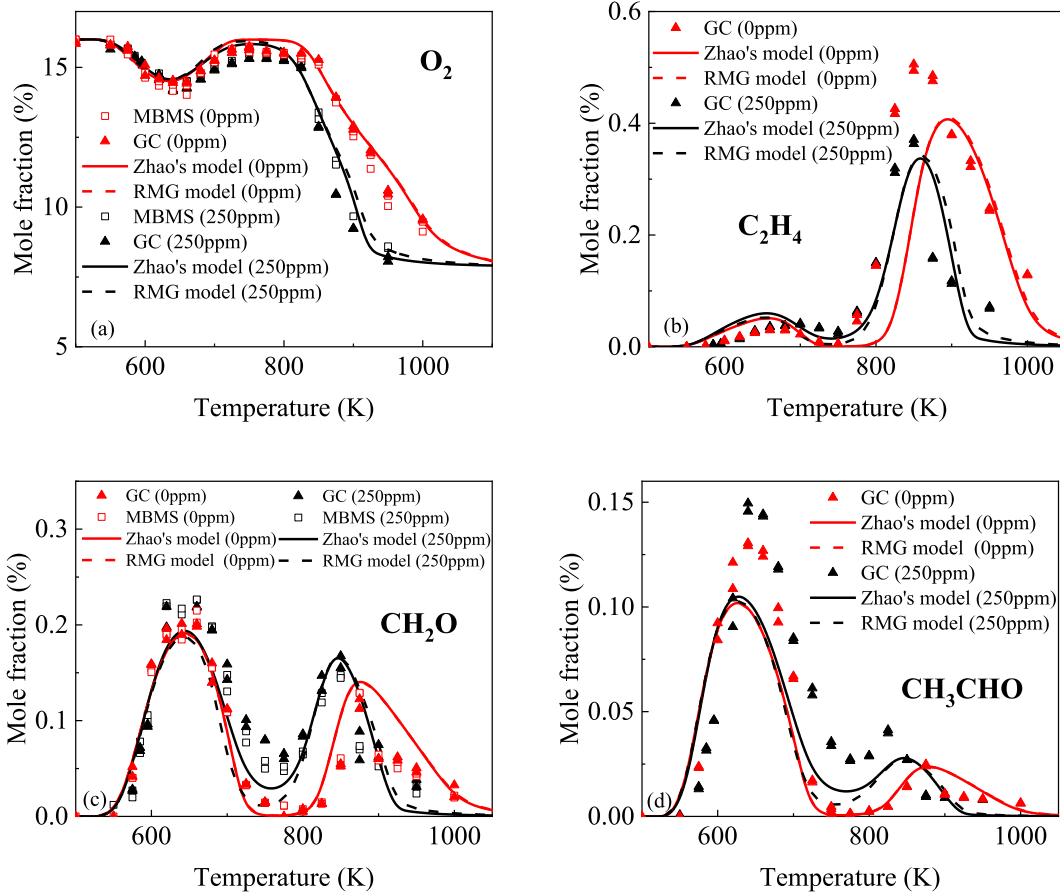


Fig. 12. Temperature evolutions of the mole fractions of O₂, C₂H₄, CH₂O, and CH₃CHO at the fuel lean conditions ($\phi=0.5$) with and without 250 ppm NO₂ addition in a JSR, conditions of Table 1.

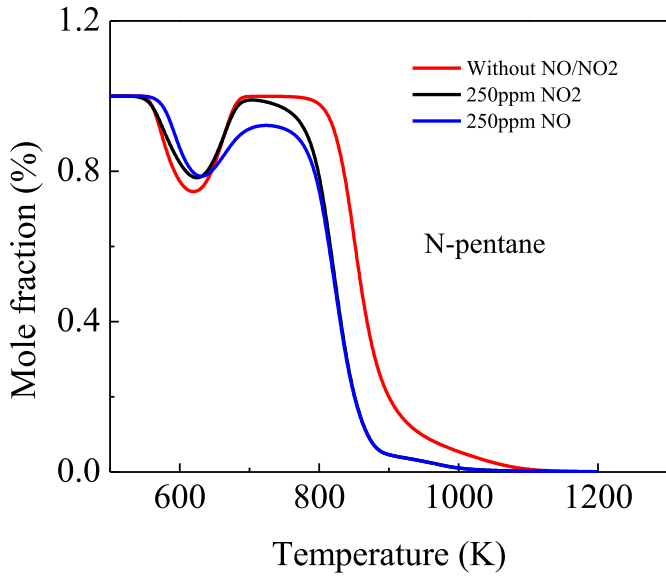


Fig. 14. Temperature evolution of the mole fraction of *n*-pentane in the fuel rich conditions ($\phi = 1.33$) with 250 ppm NO_2 , with 250 ppm NO, and without NO_2/NO additions using Zhao's model.

R_6 ; NO_2 forms HONO through R_7 , R_9 , and R_{10} ; and HONO mainly produces NO through R_{11} . The characteristic time scale of NO_x

interconversion is defined as

$$\tau_{j_1 \rightarrow j_2} = \frac{[C_{j_1}]}{\sum_{i=1}^n r_{i j_1 \rightarrow j_2}}, \quad j = \{\text{NO}, \cdot\text{NO}_2, \text{HONO}\}$$

where, $\tau_{j_1 \rightarrow j_2}$ is the characteristic time scale of j_1 to j_2 , $[C_{j_1}]$ is the volume concentration of C_{j_1} , and $r_{i j_1 \rightarrow j_2}$ is the i th reaction rate of j_1 to j_2 evaluated at steady state in JSR. At the low temperature and NTC regions (550–750 K), Conversion of NO to NO_2 is much faster than the other three characteristic time scales, and HONO decomposition is very slow. Therefore, NO is likely a QSS species and HONO is a stable molecule, which is in agreement with the NO_2 pathway analysis in Fig. 3 and NO and NO_2 mole fraction profiles in Fig. 9. Above 800 K, the conversion of NO_2 to NO becomes comparable with the time scale of NO to NO_2 , and even faster at higher temperatures. In other words, the interconversion of NO and NO_2 is very fast at this temperature range, and there is a significant dissociation of HONO to NO as well. NO, NO_2 , and HONO reach steady state quickly within the residence time in the JSR, which agrees with the pathway analysis of NO_2 in Fig. 5, and explains the similar sensitized effects of NO and NO_2 at intermediate and high temperatures in Fig. 2. Moreover, above 900 K, the time scale of NO_2 to NO is faster than that of NO to NO_2 . It explains why the NO_2 concentration decreases while NO begins to accumulate with temperature in this region. In addition, $\tau_{\text{NO} \rightarrow \text{NO}_2}$ and $\tau_{\text{NO}_2 \rightarrow \text{HONO}}$ increase at higher temperature due to a decrease in $[\text{HO}_2]$ at these conditions.

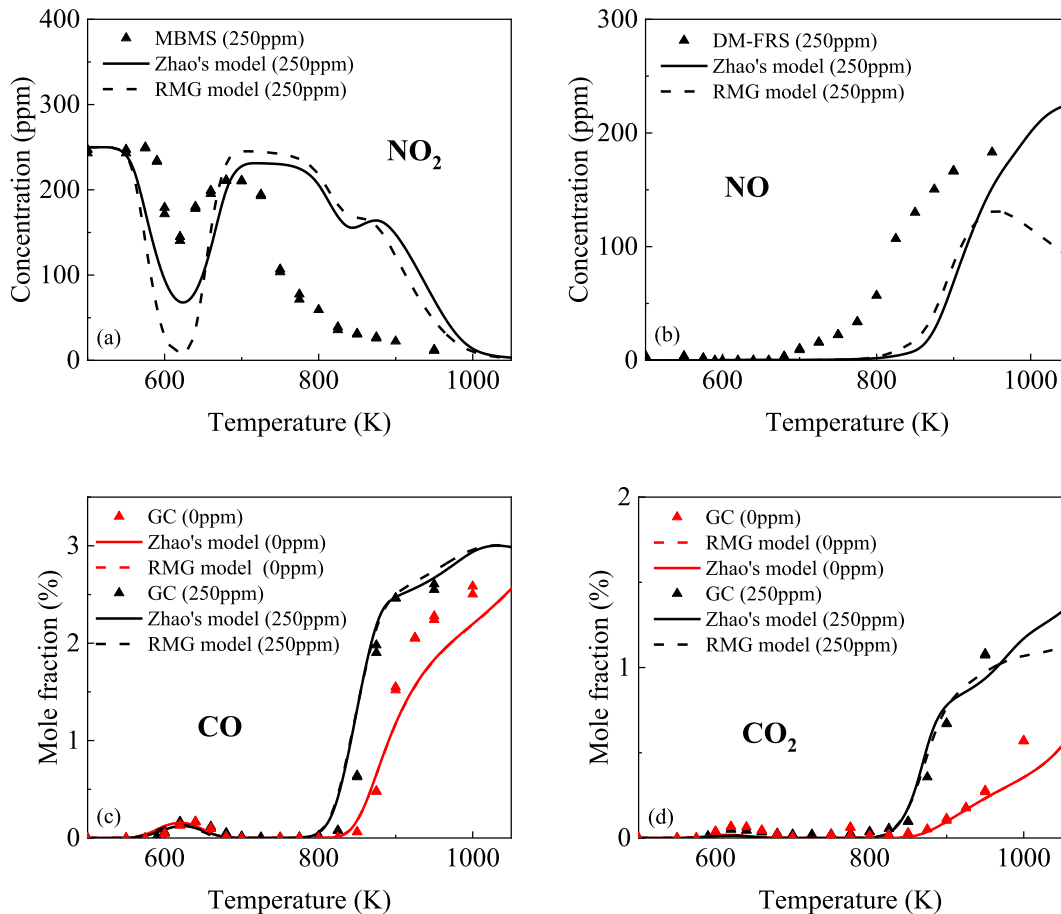


Fig. 15. Temperature evolutions of the concentrations of NO_2 , NO, CO, and CO_2 at the fuel rich conditions ($\phi = 1.33$) with and without 250 ppm NO_2 addition in a JSR, conditions of Table 1.

The temperature evolutions of O_2 , C_2H_4 , CH_2O , and CH_3CHO are shown in Fig. 12 (a)–(d), respectively. It is seen that both models predict O_2 , C_2H_4 , CH_2O , and CH_3CHO mole fraction profiles at low and high temperatures very well, indicating good model performances in capturing the pathways of the major intermediates.

Fig. 13 depicts the mole fraction of *n*-pentane versus the gas temperature at the fuel rich conditions ($\phi = 1.33$) with and without 250 ppm NO_2 addition. It is seen that the low temperature oxidation window of *n*-pentane at the fuel rich condition is much smaller than that at the lean condition in Fig. 1. According to the sensitivity analysis of *n*-pentane, $RH + OH$ is the most sensitive H abstraction reaction of *n*-pentane at low temperature. However, in the fuel rich condition, O_2 mole fraction is reduced, and reactions involving O_2 , like $RH + O_2$, $R + O_2$ and $QOOH + O_2$, are suppressed. Therefore, the low temperature oxidation is suppressed at the lower oxygen mole fraction condition. In addition, NO_2 does not have a significant weakening effect on the NTC behavior, as reaction channel R_2 is also suppressed at the condition with lower O_2 mole fraction.

Furthermore, the *n*-pentane oxidations at the fuel rich conditions with the same doping concentration of NO and NO_2 are compared in Fig. 14. Similar to the fuel lean conditions, it is seen that NO_2 addition has little effect on the onset temperature, and has less suppressive effect on the NTC behavior than NO addition at the fuel rich condition.

Fig. 15 (a)–(d) and Fig. 16 (a)–(d) depict mole fractions of NO_2 , NO , CO , CO_2 , O_2 , C_2H_4 , CH_2O , and CH_3CHO versus the gas temperature at the fuel rich conditions ($\phi = 1.33$) with and without NO_2 additions, respectively. Both models predict the mole fractions of

major intermediates and products well at low and high temperatures. However, the models still show prediction delays of the NO and NO_2 evolution curves at intermediate and high temperatures. Especially, above 925 K, unlike the experimental result and Zhao's model prediction, the predicted NO mole fraction decreases with temperature in the RMG model. NO sensitivities analysis using the RMG model (Fig. 17) shows that the uncertainty may come from reactions of $HCCO + NO = CO + HCNO$ and $HCCO + NO = CO_2 + HCN$.

4. Conclusions

The mutual oxidation of *n*-pentane and NO_2 was studied, respectively, at fuel lean and rich ($\phi = 0.5$ and 1.33) conditions with and without 250 ppm NO_2 additions at 500–1000 K. Experimental results show that at the conditions studied, NO_2 addition modestly slows oxidation below 700 K, but accelerates it at higher temperatures. First, NO_2 slows down low temperature oxidation in 550–650 K. Second, NO_2 accelerates fuel oxidation, i.e., suppresses the NTC behavior, in the NTC region (650–750 K). Furthermore, NO_2 shifts high temperature oxidation to lower temperature in the intermediate and high temperature region (750–1000 K). Two kinetic models, a newly developed RMG model and Zhao's model, were used to predict experimental results. The results show that although NO_2 addition in *n*-pentane has similar effects to NO due to fast NO and NO_2 interconversion at higher temperature, it affects low temperature oxidation somewhat differently. When NO_2/NO interconversion is slow at low temperature, NO_2 is relatively inert

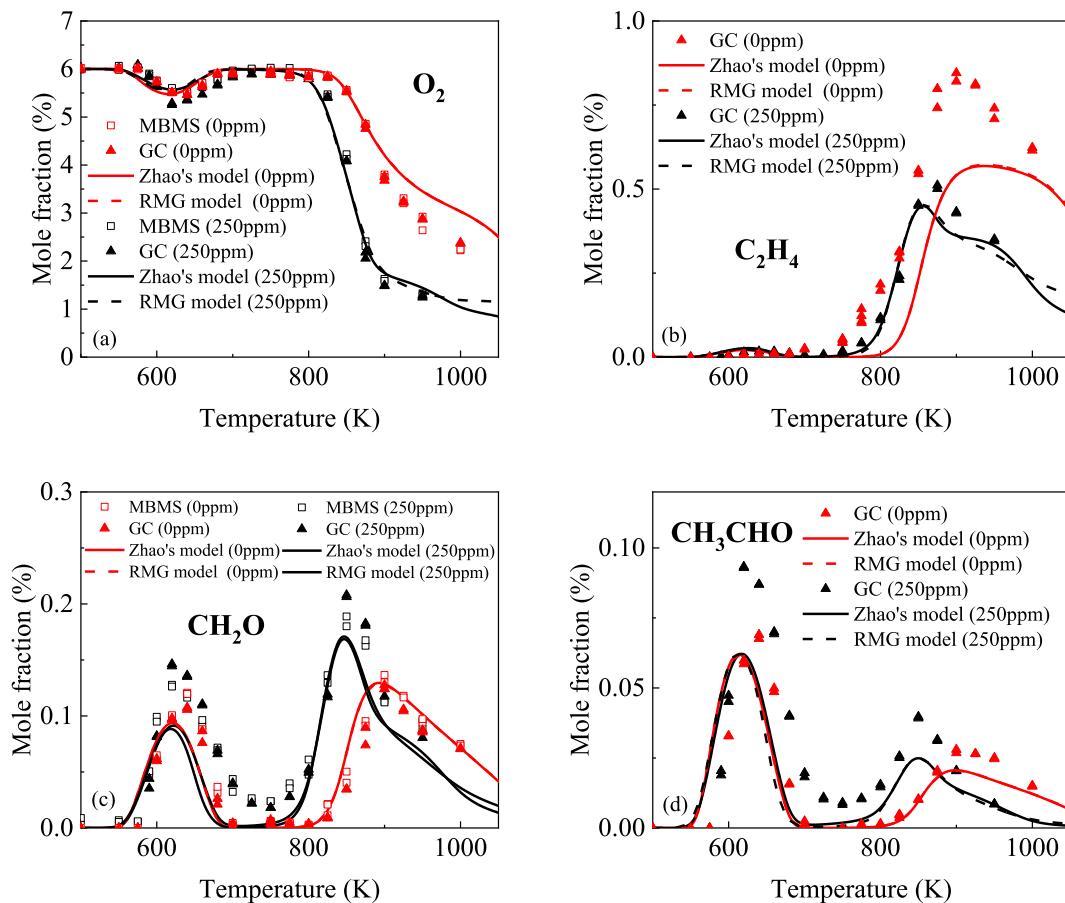


Fig. 16. Temperature evolutions of the concentrations of O_2 , C_2H_4 , CH_2O , and CH_3CHO at the fuel rich conditions ($\phi = 1.33$) with and without 250 ppm NO_2 addition in a JSR, conditions of Table 1.

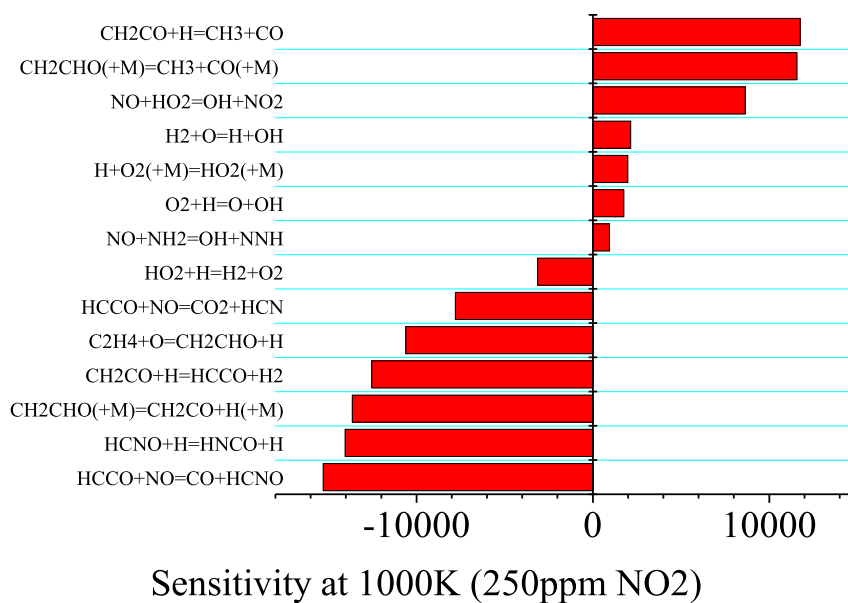


Fig. 17. Sensitivity analysis of NO at 1000 K in the fuel rich condition ($\phi = 1.33$) with 250 ppm NO₂ addition using the RMG model in a JSR, conditions of Table 1.

while NO can strongly promote or inhibit the oxidation. In addition, NO addition delays the onset temperature of *n*-pentane low temperature oxidation and strongly inhibits the NTC behavior, while NO₂ has little effect on the onset temperature and weaker impact on NTC.

Pathway analyses reveal that reactions R₁–R₃ are the dominant RO₂ consumption channels. With NO₂ addition, at 550–650 K, reaction channel R₂ inhibits *n*-pentane oxidation where the NO is primarily formed by R₄ and R₅. Nevertheless, at 650–750 K, reaction channel R₂ plays a promoting role in accelerating *n*-pentane oxidation and suppressing the NTC behavior through R₈–R₁₁. In the intermediate and high temperature regions, NO₂ addition significantly promotes high temperature oxidation through reaction channel R₃ followed by R₄ and R₈–R₁₃, and shifts it to lower temperature. Both Zhao's model and RMG model predict the experimental results reasonably well at both fuel rich and lean conditions, except for prediction delays of the NO and NO₂ evolution curves. It is suggested that the NO/NO₂ interconversion reactions are mis-predicted at 700–900 K, perhaps because additional fuel/NO_x reaction pathways are needed, or the estimated activation energies for some of the reactions involving HONO are inaccurate.

In summary, the NO_x effect on alkenes oxidation is interpreted as the following steps.

- When the oxidation is running at the temperatures with enough HO₂ and OH radicals, NO_x behaves as a catalyst, and the catalytic cycle time NO₂→NO→NO₂ is relatively short compared to the residence time in the reactor.
- At conditions where the normal oxidation chain branching is suppressed, the NO_x interconversion is slow enough that the system is sensitive to which species, NO or NO₂, is introduced. NO₂ addition has less effect on the oxidation at these conditions than NO because R₂ and R₈ are always fast but some of the NO₂ reactions are slow.

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Appendix A. Supplementary data

Supplementary data and the two kinetic models to this article can be found online at <https://doi.org/10.1016/j.energy.2018.10.013>.

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